



Basic Fluid Mechanics

Summary of introductory concepts
12 February, 2007

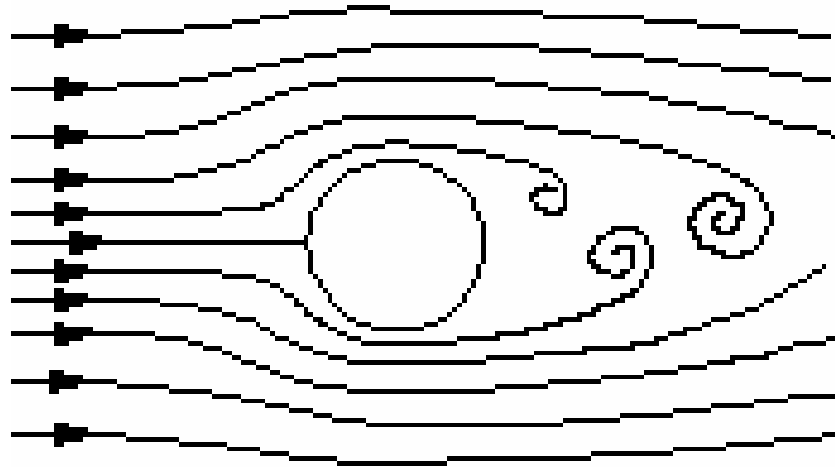
Introduction

Field of Fluid Mechanics can be divided into 3 branches:

- Fluid Statics: mechanics of fluids at rest
- Kinematics: deals with velocities and streamlines w/o considering forces or energy
- Fluid Dynamics: deals with the relations between velocities and accelerations and forces exerted by or upon fluids in motion

Streamlines

A streamline is a line that is tangential to the instantaneous velocity direction (velocity is a vector that has a direction and a magnitude)



Instantaneous streamlines in flow around a cylinder

Intro...con't

Mechanics of fluids is extremely important in many areas of engineering and science. Examples are:

- Biomechanics

- Blood flow through arteries
- Flow of cerebral fluid

- Meteorology and Ocean Engineering

- Movements of air currents and water currents

- Chemical Engineering

- Design of chemical processing equipment

Intro...con't

■ Mechanical Engineering

- Design of pumps, turbines, air-conditioning equipment, pollution-control equipment, etc.

■ Civil Engineering

- Transport of river sediments
- Pollution of air and water
- Design of piping systems
- Flood control systems

Dimensions and Units

- Before going into details of fluid mechanics, we stress importance of units
- In U.S, two primary sets of units are used:
 - 1. SI (Systeme International) units
 - 2. English units

Unit Table

Quantity	SI Unit	English Unit
Length (L)	Meter (m)	Foot (ft)
Mass (m)	Kilogram (kg)	Slug (slug) = $lb \cdot sec^2 / ft$
Time (T)	Second (s)	Second (sec)
Temperature (θ)	Celcius ($^{\circ}C$)	Farenheit ($^{\circ}F$)
Force	Newton $(N) = kg \cdot m / s^2$	Pound (lb)

Dimensions and Units con't

- 1 *Newton* – Force required to accelerate a 1 *kg* of mass to 1 m/s^2
- 1 *slug* – is the mass that accelerates at 1 ft/s^2 when acted upon by a force of 1 *lb*
- To remember units of a Newton use $F=ma$ (Newton's 2nd Law)
 - $[F] = [m][a] = kg \cdot m/s^2 = N$

More on Dimensions

- To remember units of a slug also use $F=ma \Rightarrow m = F / a$
- $[m] = [F] / [a] = lb / (ft / sec^2) = lb \cdot sec^2 / ft$
- 1 *lb* is the force of gravity acting on (or weight of) a platinum standard whose mass is 0.45359243 *kg*

Weight and Newton's Law of Gravitation

- Weight

- Gravitational attraction force between two bodies

- Newton's Law of Gravitation

$$F = G m_1 m_2 / r^2$$

- G- universal constant of gravitation
 - m_1, m_2 - mass of body 1 and body 2, respectively
 - r- distance between centers of the two masses
 - F- force of attraction

Weight

- m_2 - mass of an object on earth's surface
- m_1 - mass of earth
- r - distance between center of two masses
- r_1 - radius of earth
- r_2 - radius of mass on earth's surface
- $r_2 \ll r_1$, therefore $r = r_1 + r_2 \sim r_1$
- Thus, $F = m_2 * (G * m_1 / r^2)$

Weight

- Weight (W) of object (with mass m_2) on surface of earth (with mass m_1) is defined as

$$W = m_2 g ; g = (Gm_1/r^2) \text{ gravitational acceleration}$$

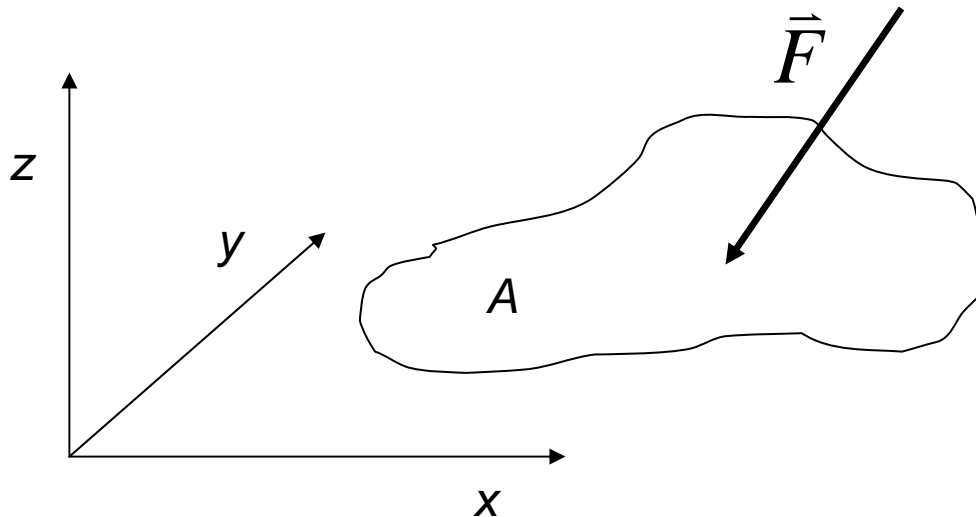
$$g = 9.31 \text{ m/s}^2 \text{ in SI units}$$

$$g = 32.2 \text{ ft/sec}^2 \text{ in English units}$$

- See back of front cover of textbook for conversion tables between SI and English units

Properties of Fluids - Preliminaries

- Consider a force, \vec{F} , acting on a 2D region of area A sitting on x-y plane



Cartesian components: $\vec{F} = F_x (\pm \hat{i}) + F_y (\pm \hat{j}) + F_z (\pm \hat{k})$

Cartesian components

$\pm \hat{i}$ - Unit vector in $\pm x$ -direction

$\pm \hat{j}$ - Unit vector in $\pm y$ -direction

$\pm \hat{k}$ - Unit vector in $\pm z$ -direction

F_x - Magnitude of \vec{F} in $\pm x$ -direction (tangent to surface)

F_y - Magnitude of \vec{F} in $\pm y$ -direction (tangent to surface)

F_z - Magnitude of \vec{F} in $\pm z$ -direction (normal to surface)

- For simplicity, let $F_y = 0$

- Shear stress and pressure

$$\tau = \frac{F_x}{A} \quad (\textit{shear stress})$$

$$p = \frac{F_z}{A} \quad (\textit{normal stress (pressure)})$$

- Shear stress and pressure at a point

$$\tau = \left(\frac{F_x}{A} \right)_{\lim A \rightarrow 0} \qquad p = \left(\frac{F_z}{A} \right)_{\lim A \rightarrow 0}$$

- Units of stress (shear stress and pressure)

$$\frac{[F]}{[A]} = \frac{N}{m^2} = Pa \text{ (Pascal) in SI units}$$

$$\frac{[F]}{[A]} = \frac{lb}{in^2} = psi \text{ (pounds per square inch) in English units}$$

$$\frac{[F]}{[A]} = \frac{lb}{ft^2} = \text{pounds per square foot (English units)}$$

Properties of Fluids Con't

- Fluids are either liquids or gases
- Liquid: A state of matter in which the molecules are relatively free to change their positions with respect to each other but restricted by cohesive forces so as to maintain a relatively fixed volume
- Gas: a state of matter in which the molecules are practically unrestricted by cohesive forces. A gas has neither definite shape nor volume.




More on properties of fluids

- Fluids considered in this course move under the action of a shear stress, no matter how small that shear stress may be (unlike solids)

Continuum view of Fluids

- Convenient to assume fluids are continuously distributed throughout the region of interest. That is, the fluid is treated as a continuum
- This continuum model allows us to not have to deal with molecular interactions directly. We will account for such interactions indirectly via viscosity
- A good way to determine if the continuum model is acceptable is to compare a characteristic length (L) of the flow region with the mean free path of molecules, λ
- If $L \ll \lambda$, continuum model is valid

- 
- Mean free path (λ) – Average distance a molecule travels before it collides with another molecule.

1.3.2 Density and specific weight

Density (mass per unit volume): $\rho = \frac{m}{V}$

Units of density: $[\rho] = \frac{[m]}{[V]} = \frac{kg}{m^3}$ (in SI units)

Specific weight (weight per unit volume): $\gamma = \rho g$

Units of specific weight:

$$[\gamma] = [\rho][g] = \frac{kg}{m^3} \frac{m}{s^2} = \frac{N}{m^3} \quad (\text{in SI units})$$

Specific Gravity of Liquid (S)

$$S = \frac{\rho_{liquid}}{\rho_{water}} = \frac{\rho_{liquid} g}{\rho_{water} g} = \frac{\gamma_{liquid}}{\gamma_{water}}$$

- See appendix A of textbook for specific gravities of various liquids with respect to water at 60 °F

1.3.3 Viscosity (μ)

- Viscosity can be thought as the internal stickiness of a fluid
- Representative of internal friction in fluids
- Internal friction forces in flowing fluids result from cohesion and momentum interchange between molecules.
- Viscosity of a fluid depends on temperature:
 - In liquids, viscosity decreases with increasing temperature (i.e. cohesion decreases with increasing temperature)
 - In gases, viscosity increases with increasing temperature (i.e. molecular interchange between layers increases with temperature setting up strong internal shear)

More on Viscosity

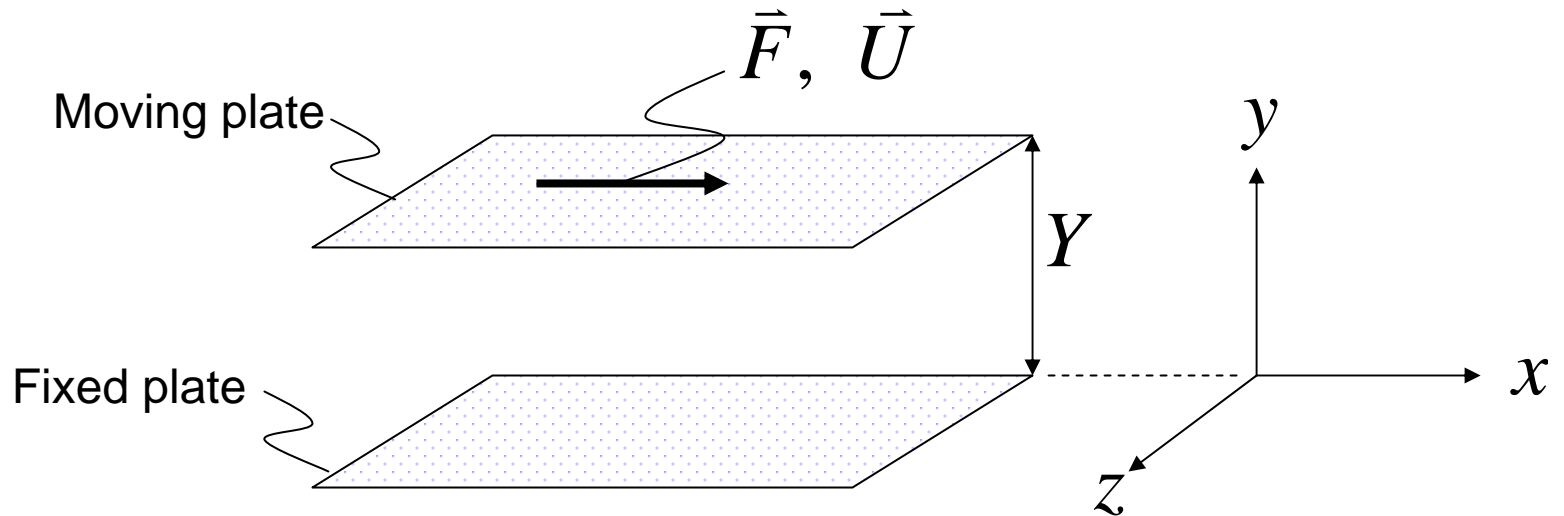
- Viscosity is important, for example,
 - in determining amount of fluids that can be transported in a pipeline during a specific period of time
 - determining energy losses associated with transport of fluids in ducts, channels and pipes

No slip condition

- Because of viscosity, at boundaries (walls) particles of fluid adhere to the walls, and so the fluid velocity is zero relative to the wall
- Viscosity and associated shear stress may be explained via the following: flow between no-slip parallel plates.

Flow between no-slip parallel plates

-each plate has area A

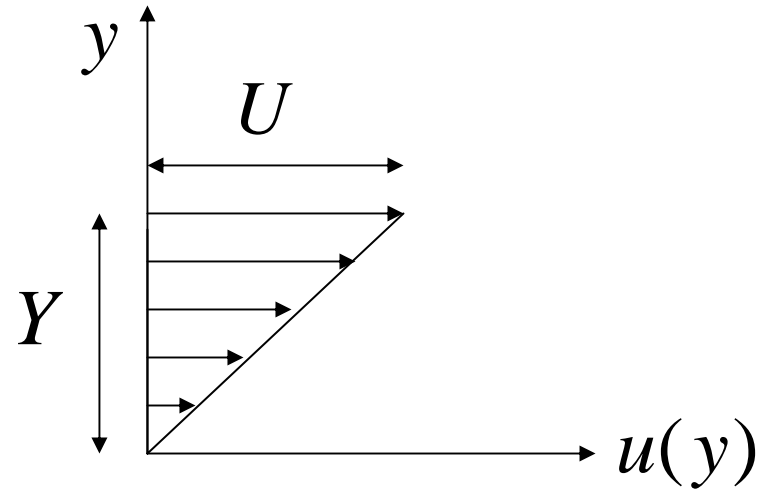


$$\vec{F} = F\hat{i} \quad \vec{U} = U\hat{i}$$

Force \vec{F} induces velocity \vec{U} on top plate. At top plate flow velocity is \vec{U}

At bottom plate velocity is $\mathbf{0}$

The velocity induced by moving top plate can be sketched as follows:



$$u(y = 0) = 0$$

$$u(y = Y) = U$$

The velocity induced by top plate is expressed as follows:

$$u(y) = \left(\frac{U}{Y} \right) y$$

For a large class of fluids, empirically, $F \propto \frac{AU}{Y}$

More specifically, $F = \mu \frac{AU}{Y}$; μ is coefficient of viscosity

Shear stress induced by F is $\tau = \frac{F}{A} = \mu \frac{U}{Y}$

From previous slide, note that $\frac{du}{dy} = \frac{U}{Y}$

Thus, shear stress is $\tau = \mu \frac{du}{dy}$

In general we may use previous expression to find shear stress at a point inside a moving fluid. Note that if fluid is at rest this stress is zero because $\frac{du}{dy} = 0$

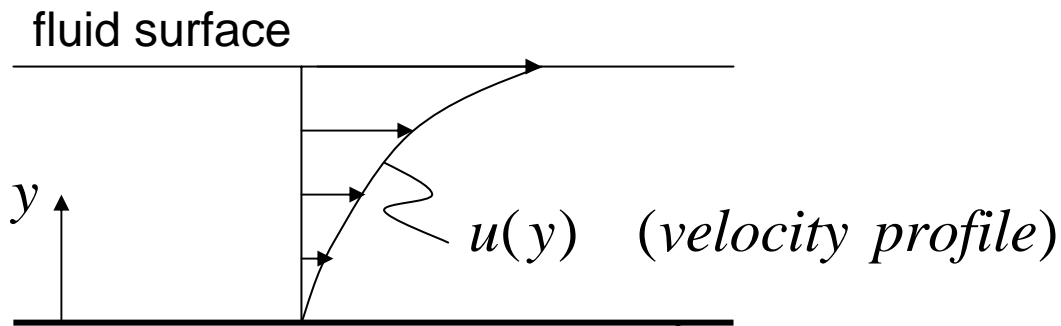
Newton's equation of viscosity

Shear stress due to viscosity at a point:

$$\tau = \mu \frac{du}{dy}$$

μ - viscosity (coeff. of viscosity)

$\nu = \frac{\mu}{\rho}$ - kinematic viscosity



e.g.: wind-driven flow in ocean

Fixed no-slip plate

As engineers, Newton's Law of Viscosity is very useful to us as we can use it to evaluate the shear stress (and ultimately the shear force) exerted by a moving fluid onto the fluid's boundaries.

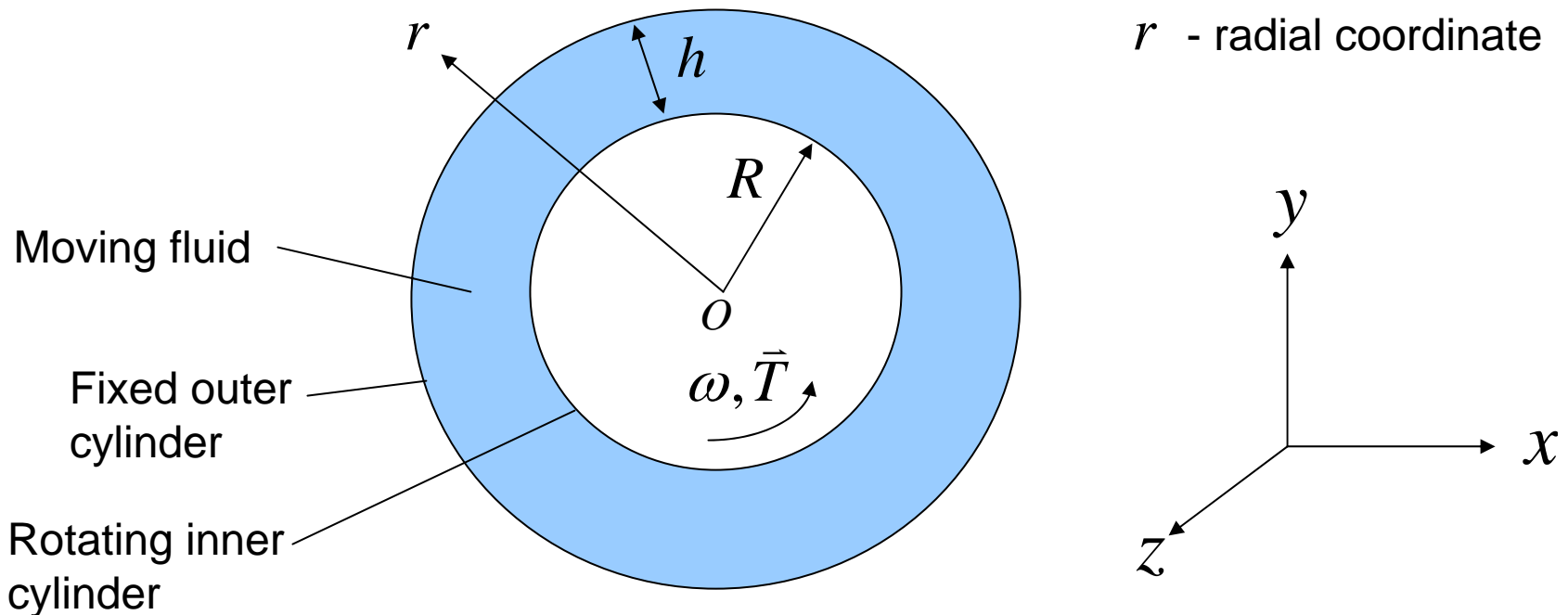
$$\tau \text{ at boundary} = \mu \left(\frac{du}{dy} \right)_{\text{at boundary}}$$

Note y is direction normal to the boundary

Viscometer

Coefficient of viscosity μ can be measured empirically using a viscometer

Example: Flow between two concentric cylinders (viscometer) of length L



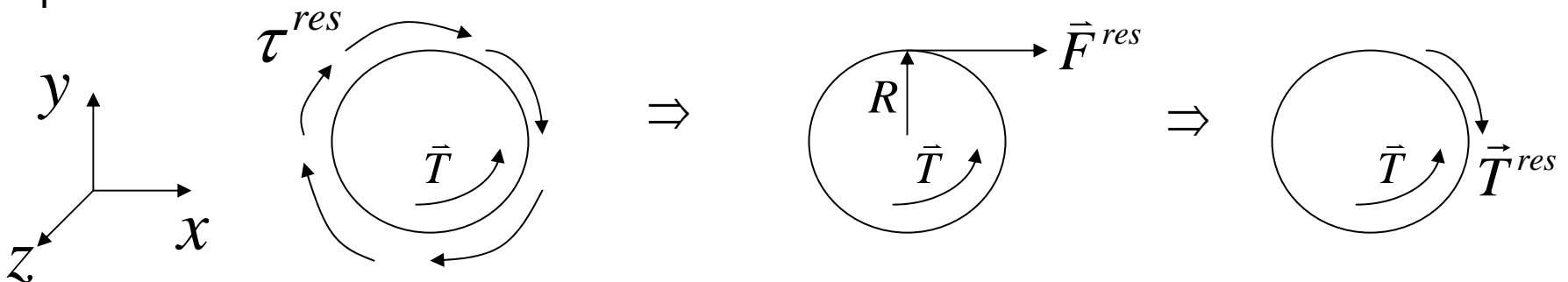
Inner cylinder is acted upon by a torque, $\vec{T} = T \hat{k}$, causing it to rotate about point O at a constant angular velocity ω and causing fluid to flow. Find an expression for \vec{T}

Because ω is constant, $\vec{T} = T \hat{k}$ is balanced by a resistive torque exerted by the moving fluid onto inner cylinder

$$T = T^{res}$$

$$\vec{T}^{res} = T^{res} (-\hat{k})$$

The resistive torque comes from the resistive stress τ^{res} exerted by the moving fluid onto the inner cylinder. This stress on the inner cylinder leads to an overall resistive force \vec{F}^{res} , which induces the resistive torque about O point



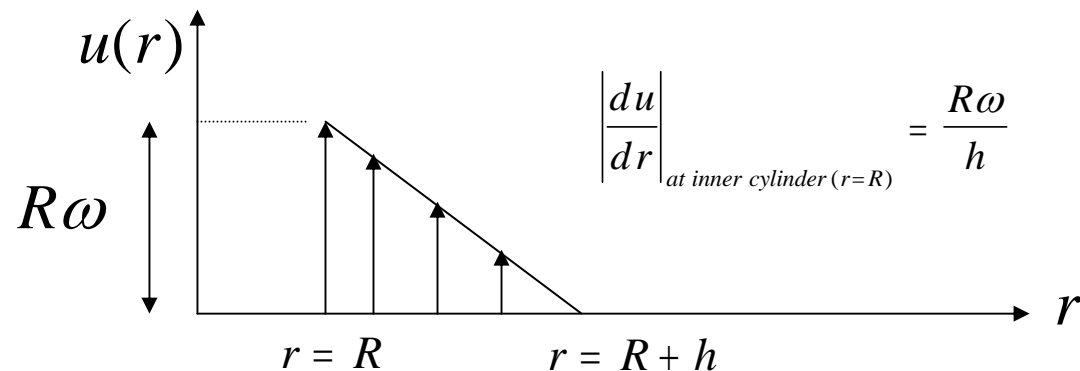
$$T = T^{res} = F^{res} R$$

$$F^{res} = \tau^{res} A = \tau^{res} (2\pi R L) \quad (\text{Neglecting ends of cylinder})$$

How do we get τ^{res} ? This is the stress exerted by fluid onto inner cylinder, thus

$$\tau^{res} = \mu \left. \frac{du}{dr} \right|_{\text{at inner cylinder } (r=R)}$$

If h (gap between cylinders) is small, then



Thus, $\tau^{res} = \mu \frac{R\omega}{h}$

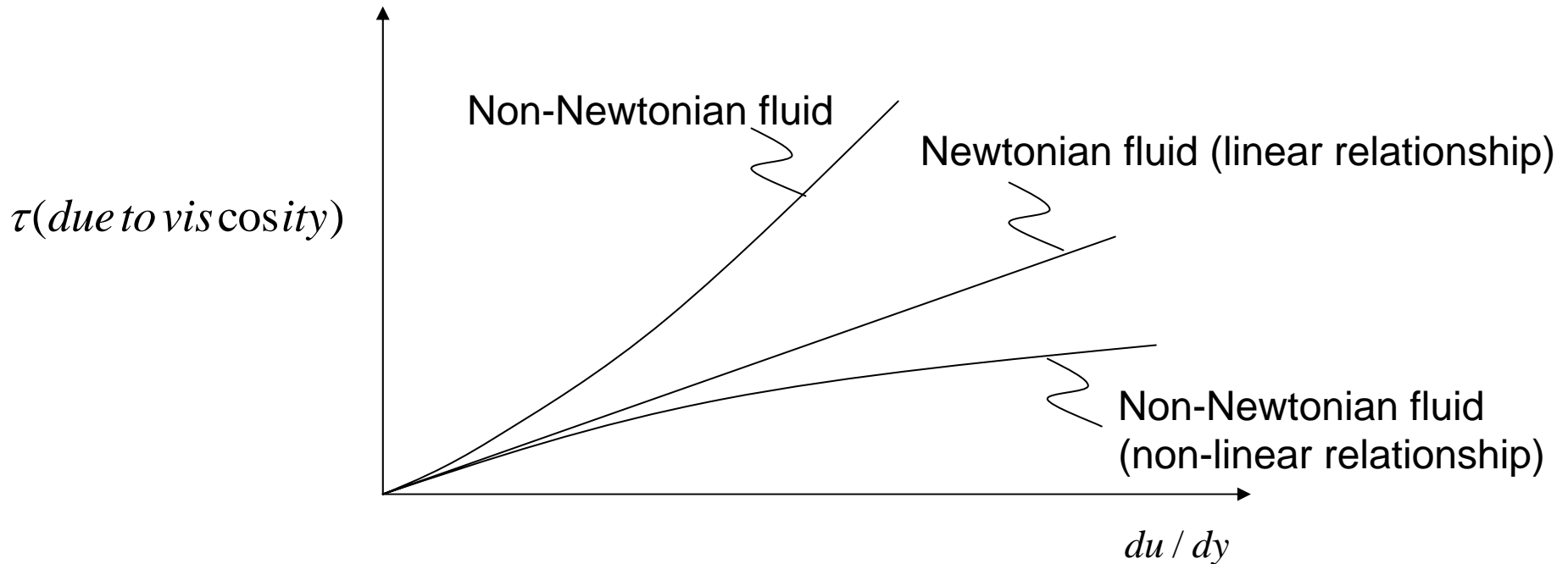
$$T = T^{res} = F^{res} R$$

$$T = T^{res} = \tau^{res} AR = \tau^{res} (2\pi R L) R$$
$$= \mu \left(\frac{R\omega}{h} \right) (2\pi R L) R$$

$$T = \frac{R^3 \mu \omega 2\pi L}{h}$$

Given T, R, ω, L, h previous result may be used to find μ of fluid, thus concentric cylinders may be used as a viscometer

Non-Newtonian and Newtonian fluids



- In this course we will only deal with Newtonian fluids
- **Non-Newtonian fluids:** blood, paints, toothpaste

Compressibility

- All fluids compress if pressure increases resulting in an increase in density
- Compressibility is the change in volume due to a change in pressure
- A good measure of compressibility is the bulk modulus (It is inversely proportional to compressibility)

$$E_v = -v \frac{dp}{dv} \qquad v = \frac{1}{\rho} \quad (\text{specific volume})$$

p is pressure

Compressibility

- From previous expression we may write

$$\frac{(v_{final} - v_{initial})}{v_{initial}} \approx - \frac{(p_{final} - p_{initial})}{E_v}$$

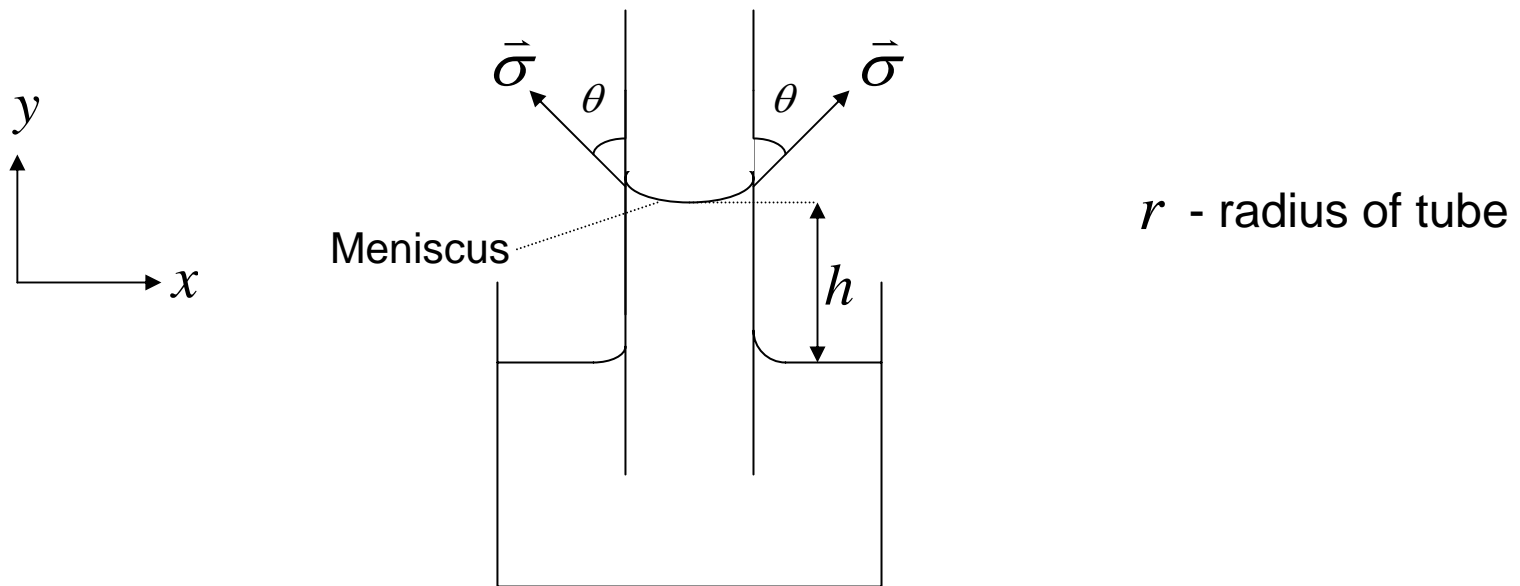
- For water at 15 *psia* and 68 degrees Fahrenheit, $E_v = 320,000 \text{ psi}$
- From above expression, increasing pressure by 1000 *psi* will compress the water by only 1/320 (0.3%) of its original volume
- Thus, water may be treated as **incompressible (density (ρ) is constant)**
- In reality, no fluid is incompressible, but this is a good approximation for certain fluids

Vapor pressure of liquids

- All liquids tend to evaporate when placed in a closed container
- Vaporization will terminate when equilibrium is reached between the liquid and gaseous states of the substance in the container
 - i.e. # of molecules escaping liquid surface = # of incoming molecules
- Under this equilibrium we call the call vapor pressure the saturation pressure
- At any given temperature, if pressure on liquid surface falls below the the saturation pressure, rapid evaporation occurs (i.e. boiling)
- For a given temperature, the saturation pressure is the boiling pressure

Surface tension

- Consider inserting a fine tube into a bucket of water:



$\vec{\sigma}$ - Surface tension vector (acts uniformly along contact perimeter between liquid and tube)

Adhesion of water molecules to the tube dominates over cohesion between water molecules giving rise to $\vec{\sigma}$ and causing fluid to rise within tube

$$\vec{\sigma} = \sigma \hat{n}$$

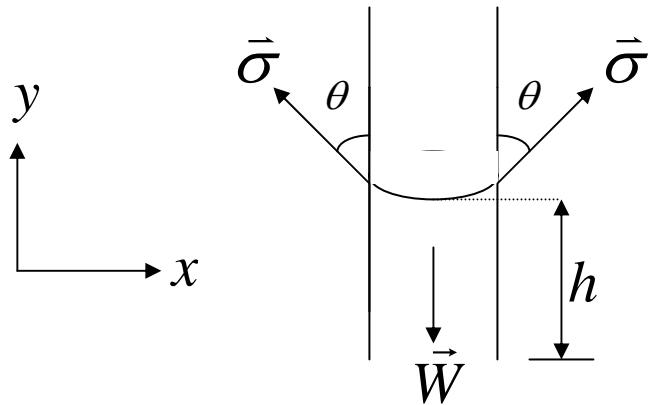
\hat{n} - unit vector in direction of $\vec{\sigma}$

σ - surface tension (magnitude of $\vec{\sigma}$)

$$\vec{\sigma} = \sigma [\sin \theta(\hat{i}) + \cos \theta(\hat{j})]$$

$$[\sigma] = \frac{\text{force}}{\text{length}}$$

Given conditions in previous slide, what is σ ?



$$\vec{\sigma} = \sigma [\sin \theta (\hat{i}) + \cos \theta (\hat{j})]$$

$$\vec{W} = W (-\hat{j}) \quad (\text{weight vector of water})$$

Equilibrium in *y-direction* yields: $\sigma \cos \theta (2\pi r) (\hat{j}) + W(-\hat{j}) = 0 \hat{j}$

Thus

$$\sigma = \frac{W}{2\pi r \cos \theta}$$

with $W = \gamma_{\text{water}} \pi r^2 h$